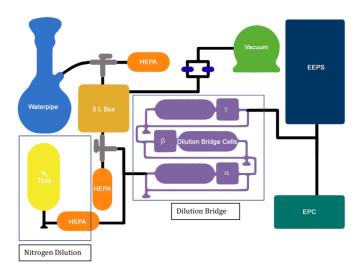
Supplementary material Tob Control



**Dilution Factor Calculation** 

The theoretical dilution factor  $(D_t)$  is defined as the product of the dilution due to the dilution bridges  $(D_F)$ , the dilution due to the box  $(D_B)$ , and the dilution due to the nitrogen  $(D_N)$  (Eq.1).

$$D_T = D_F * D_B * D_N \tag{1}$$

The  $D_F$  is defined as the product of the dilution factor of the bridge cells ( $D_\alpha$ ,  $D_\beta$ ,  $D_\gamma$ ) (Eq. 2).

$$D_F = D_{\alpha} * D_{\beta} * D_{\gamma} \tag{2}$$

 $D_{\alpha}$ ,  $D_{\beta}$ ,  $D_{\gamma}$  is determined from the maximum flow  $(F_{M,k})$  and the filtered flow  $(F_k)$  (Eq. 3).

$$D_k = \frac{F_{M,k}}{F_{M,k} - F_k}; \ k = \alpha, \beta, \gamma, N \quad (3)$$

The maximum flow through bridges A, B, and C was experimentally determined to be 11.17 LPM, 10.69 LPM, and 10.64 LPM respectively.

Mixing the filtered air present in the box during the puff.  $D_B$  can be determined from the volume of the box and the volume of the puff (Eq. 4).

$$D_B = V_B * t_{Puff} * Puff Rate$$
 (4)

Similar to the determination of the dilution factor of a dilution bridge, the dilution factor due to nitrogen  $(D_N)$  can be calculated by from the max flow and the measured nitrogen flow (Eq. 5).

$$d_N = \frac{A_m}{(A_m - N)} \tag{5}$$

60 minute calibration runs were performed using a medium pipe, Teflon and glycerol in the head, and charcoal to determine the linear relationship between the  $D_t$  and the experimental dilution factor ( $D_E$ ). The PM was both sampled in the box and after the dilution bridges. After three trials, a relationship of  $D_t$  = 1.0674\*  $D_E$  -0.5394 (R=0.8493) was determined.

Figure S1. Experimental apparatus for physical properties determination with dilution construct including bridge and nitrogen dilutant highlighted.